

We claim:

1. A process for preparing riboflavin of the B/C modification in granule form, which comprises

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- a) dissolving riboflavin of the A modification in aqueous mineral acid,
- b) directly afterwards, without initially treating the resulting riboflavin solution in mineral acid with activated carbon, precipitating, steps a) and b) being carried out at a temperature in the range from 5 to 15°C, and
- 10 c) drying the riboflavin by fluidized bed spray granulation.

2. A process as claimed in claim 1, wherein the dissolution temperature is selected within the range from 5 to 12°C.

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3. A process as claimed in either of claims 1 and 2, wherein the riboflavin does not come into contact with the aqueous mineral acid solvent for longer than on average 4 h.

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4. A process as claimed in any of claims 1 to 3, wherein the riboflavin does not come into contact with the aqueous mineral acid solvent for longer than on average 3 h.

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5. A process as claimed in any of claims 1 to 4, wherein the precipitation is carried out within a temperature range from 6 to 12°C.

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A process as claimed in any of claims 1 to 5, wherein the precipitation is carried out continuously.

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7. A process as claimed in any of claims 1 to 6, wherein the precipitation is carried out in a two-stage stirred tank battery.

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8. A process as claimed in any of claims 1 to 7, wherein the precipitation is carried out in the first stirred tank of the two-stage stirred tank battery with an average residence time of the riboflavin solution in the first stirred tank of from 1 to 10 min.

9. A process as claimed in any of claims 1 to 8, wherein drying is carried out using a continuous or semicontinuous fluidized bed spray granulation in top-spray configuration.

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10. A process as claimed in any of claims 1 to 9, wherein the temperature of the dry gas blown into the dryer in the fluidized bed spray granulation is in the range from 100 to 200°C.
- 5 11. A process as claimed in any of claims 1 to 10, wherein the temperature of the dry gas blown into the dryer in the fluidized bed spray granulation is in the range from 150 to 170°C.
- 10 12. A process as claimed in any of claims 1 to 11, wherein a portion of the riboflavin obtained after the drying is recycled back into the drying process, and the ratio of the stream recycled into the spray fluidized bed to the stream which is removed from the process as the product of value is from about 1:1 to about 4:1.
- 15 13. Riboflavin in granule form which has a bulk density of from 0.45 to 0.7 g/ml (DIN 53468) and, after tabletting, has a dissolution of at least 80%.
- 20 14. Riboflavin as claimed in claim 13 having a bulk density of from 0.5 to 0.65 g/ml.
15. Riboflavin as claimed in claim 14 which, after tabletting, has a dissolution of at least 85%.
- 20 16. Riboflavin as claimed in any of claims 13 to 15 which comprises no binder.
17. Tablets produced using the riboflavin as claimed in any of claims 13 to 16.